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Carbon nitride nanotubes anchored with high-density CuN_x sites for efficient degradation of antibiotic contaminants under photo-Fenton process: Performance and mechanism

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ABSTRACT

The low specific surface area, poor porosity, and weak charge transport caused by the disordered morphology of metal-N-site catalysts are the main factors limiting their environmental applications. Therefore, a hollownanotube carbon nitride (Cu-HNCN) catalyst with CuN_x sites dispersed in a hollow nanotube-like CN was constructed and used for the degradation of organic pollutants via the photo-Fenton (PF) process. The high specific surface area, rich porosity, and good visible-light trapping capability of the Cu-HNCN nanotubes were identified. The Cu-HNCN/PF system achieved 96.0% degradation efficiency of tetracycline within 50 min and showed efficient degradation of various antibiotic contaminants. Moreover, the short Cu-N bonds contributed to the improved stability and decreased copper leaching in the Cu-HNCN/PF system. Cu-HNCN, with its enhanced photogenerated charge generation, separation, and transport, was the key to the generation of abundant active species and efficient degradation of pollutants. In addition, frontier electron density theory successfully distinguished the roles of different types of active species in the degradation process. This work provides new insights into the development of catalysts with high stability and accelerated electron transfer to enhance the application of the PF process in practical wastewater purification.

1. Introduction

Antibiotics are commonly used in clinical medicine and animal husbandry and are frequently detected in the environment because they are difficult to biodegrade [1,2]. Antibiotic contaminants and their derivatives can cause the spread of multidrug resistance in the environment, leading to the emergence of drug-resistant genes or bacteria and posing a potential threat to human health and the environment [3,4]. Hence, effective technologies for the treatment of antibiotic contaminants must be developed to reduce environmental risks. Advanced oxidation processes (AOPs) are currently one of the most attractive methods for the treatment of refractory organics, as they activate various peroxides to generate reactive oxygen species (ROS) such as free radicals or singlet oxygen [5,6]. These ROS can effectively mineralize

hard-to-degrade pollutants into carbon dioxide and water.

Fenton oxidation based on hydroxyl radicals (\cdot OH) has been extensively investigated for the removal of refractory pollutants because of its excellent redox potential ($E^0=2.73$ V) and strong electrophilic addition property of OH [7]. Moreover, the heterogeneous Fenton-like reaction has the advantages of easy catalyst separation, which avoids metal leakage, and environmental compatibility, overcoming the defects of traditional homogeneous Fenton technology [8]. However, the monotonic Fenton-like reaction is limited by H_2O_2 activation efficiency, which limits its applicability in environmental remediation. In general, the medium for the activation of H_2O_2 to form OH in Fenton-like reactions is the redox cycle of $M^{n+}/M^{(n+1)+}$ (where M represents the transition metal atoms), and the rate-limiting step is the reduction of $M^{(n+1)+}$ to M^{n+} [9,10]. The heterogeneous visible-light photo-assisted

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photo-Fenton (PF) system can enhance the regeneration of subvalent M^{n+} and thus promote H_2O_2 activation through the synergistic effect of green photocatalytic technology and Fenton-like reactions [11,12]. The mechanism of the PF process includes (1) the capture of light energy by the catalyst and photogeneration of electrons, which promote the regeneration of subvalent M^{n+} activators, thus advancing the Fenton-like reaction; (2) effective consumption of photogenerated electrons and release of holes with strong oxidative capability by the optimized electron-hole pair separation, promoting photocatalytic oxidation [13,14]. The PF process can enhance the catalytic rate and mineralization of refractory pollutants owing to its intrinsic synergistic steps.

Copper-based catalysts, which have attracted considerable attention owing to their unique valence electron structures, are widely used as H₂O₂ activators [15,16]. Copper, copper oxides, copper sulfides, and copper-containing polymetallic compounds have been evaluated as catalysts for Fenton-like reactions [17-20]. Catalytic reactions are generally more dependent on isolated atoms than on atoms, emphasizing the utilization of metal atoms [21]. However, the precise synthesis of highly dispersed metal catalysts remains challenging because of the natural diffusion and agglomeration of metal atoms during the synthesis process [22,23]. In addition, catalytic reactions usually occur on the catalyst surface, and unstable metal-carrier interactions can cause metal leaching. Therefore, suitable catalysts with highly dispersed and stable active metal sites must be developed. Graphitic carbon nitride (CN) exhibits the advantages of visible-light response, easy synthesis, non-toxicity, and high stability [24,25]. Its unique "six-fold cavity" with lone electron pair N coordination can provide strong interactions with metal atoms, forming stable metal-N (MN_x) sites, thus achieving highly dispersed metal sites and effectively avoiding leaching due to direct exposure of metals [26,27]. In addition, the heterostructure (Cu-N) can effectively reduce the surface Cu(II) [28,29]. Therefore, CN-based catalysts with CuNx sites are considered promising for the degradation of refractory pollutants in the PF reaction.

However, primitive CN carriers suffer from defects such as low specific surface area, low porosity, weak charge transport capacity, and insufficient exposure of active centers owing to their disordered twodimensional (2D) phases [25,30,31]. Notably, nanostructure design, that is, changes in size in certain directions, which lead to changes in quantum confinement, results in highly anisotropic low-dimensional materials with dramatic changes in the electronic structure and physical and chemical properties [32,33]. Hollow nanostructured materials have demonstrated promising applications in heterogeneous catalytic reactions owing to their optimized light trapping and oxidation/reduction species separation [34]. The separation efficiency of photogenerated charges in the hollow nanospheric CN is significantly higher than that in the disordered bulk CN [35]. Moreover, the hollow nanostructure can cause multiple reflections of incident light in the catalyst cavity, thus promoting the utilization of light in the PF reaction. The construction of 1D structural morphology engineering can enlarge the specific surface area of the catalyst and the exposure efficiency of the active sites and provide a pathway for the directional transfer of electrons [36,37], both of which are beneficial for redox reactions that depend on electron transport. Predictably, morphological engineering can achieve high specific surface area, high porosity, efficient light trapping, and fast charge transport of CN carriers [38,39]. Therefore, anchoring Cu species to hollow-nanotube CN (Cu-HNCN) carriers is considered to have the following advantages: (1) enhanced visible-light utilization efficiency, (2) high specific surface area and exposed metal active sites, (3) strong metal-carrier interactions, and (4) excellent charge separation and transport properties. However, the construction of metal-anchored catalysts with 1D and hollow morphologies remains challenging because coatings with highly curved surfaces are difficult to control [40]. However, once prepared, such catalysts may become outstanding environmentally functional materials with practical application potential.

In this study, Cu-HNCN catalysts with highly dispersed CuN_x sites were prepared and used as PF catalysts for the degradation of antibiotic contaminants. Tetracycline (TET), which is widely used and released into the environment as an animal growth promoter to enhance growth rate and feed conversion, was selected as a model contaminant [41]. Characterization determined the morphological structure and form of active sites present in the Cu-HNCN catalyst. The effects of H2O2 concentration, catalyst dosage, pH, TET concentration, coexisting substances, and the real water matrix on TET degradation during the PF process were investigated. Density functional theory (DFT) calculations clarified the configuration of Cu-HNCN and the role of the morphological structure in charge transport. Various active substances and their roles in the reaction were identified and a catalytic degradation mechanism was proposed. Finally, the TET degradation pathway was proposed based on frontier electron density (FED) calculations and liquid chromatography-mass spectrometry (LC-MS).

2. Materials and methods

2.1. Materials

The source and type of materials used are provided in Supporting Material Text S1.

2.2. Synthesis of catalysts

HNCN was prepared according to a modified method reported by Xu et al. [35]. First, 2 g melamine and 2 g cyanuric acid were dissolved in 40 ml deionized water, mixed, and stirred at room temperature for 10 min. Then, the mixed solution was placed in a 150 ml autoclave with a polytetrafluoroethylene lining and kept at 200 °C for 12 h under magnetic stirring. The obtained intermediate was dried under vacuum at 60 °C. Finally, the product was fully ground, placed in a covered ceramic crucible, heated to 550 °C at 5 °C/min under nitrogen, and maintained for 4 h. The final product was obtained by natural cooling.

The Cu-HNCN catalyst was prepared by a similar procedure. A total of 0.303 g Cu(NO $_3$) $_2$.3 H $_2$ O was weighed, dissolved in 10 ml deionized water, and sonicated for 10 min. The copper source solution was then added dropwise to a mixture of 2 g melamine and 2 g cyanuric acid. The subsequent steps were the same as those used for preparing HNCN. The final product was denoted as 2Cu-HNCN (where 2 represents the mass percentage of Cu/melamine + cyanuric acid).

Disordered CN and Cu-anchored CN (Cu-CN) were prepared using a similar method without hydrothermal treatment, and the mixed solution was stirred at 100 $^{\circ}\text{C}$ until the moisture was completely removed and then calcined following the same procedure.

2.3. Characterizations

The characterization instruments and parameters used for the catalyst characterization are provided in Supporting Material Text S2.

2.4. Catalytic performance evaluation

All degradation processes were carried out in a 150 ml quartz reactor, which was equipped with circulating water to maintain the reaction temperature at 20 °C. The TET concentration was 10 mg/L. After the catalyst was added, the reaction gel was pre-stirred for 30 min in the dark to reach the adsorption–desorption equilibrium. Then, $\rm H_2O_2$ was added, and the light source was turned on to initiate the degradation process. The light source was a 300 W xenon lamp (CEL-HXF300, CEAULIGHT, China) equipped with a filter (>420 nm), and the light density was maintained at 100 mW/cm². At a preset time, a 3 ml sample was obtained and passed through a 0.22 μm filter membrane. The initial pH was adjusted using 0.1 M HCl or 0.1 M NaOH. The catalytic reaction kinetics were obtained using a fitted first-order reaction kinetics

equation. In Eq. (1), C_0 represents the initial concentration of the pollutants, C_t denotes the real-time concentration of the pollutants, and $k_{\rm obs}$ is the rate constant of the fitted first-order kinetics. The catalyst was then collected via centrifugation.

$$-\ln\left(\frac{C_t}{C_0}\right) = k_{obs} \tag{1}$$

2.5. Analytical methods

All information on the equipment model and experimental methods is provided in Supporting Material Text S3.

2.6. Theoretical computation

The details of the theoretical computation are provided in Supporting Material Text S4.

3. Results and discussion

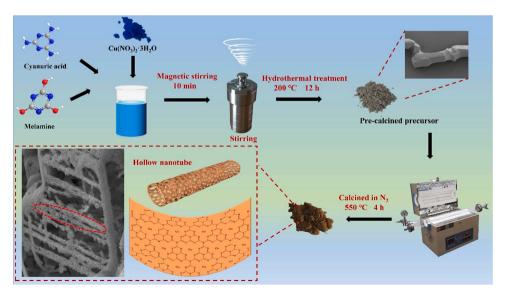
3.1. Characterization

3.1.1. Morphology and structural analysis

As shown in Scheme 1, the Cu-HNCN catalyst was prepared using Cu (NO₃)₂.3 H₂O, melamine, and cyanuric acid as the raw materials. Fig. 1a and b show the apparent morphology of the precursor after hydrothermal treatment. The precursor sample exhibited a regular cavity composed of multiple reduced 2D planes with a cavity diameter of approximately 5.8 µm. Notably, the morphology of the sample changed significantly after calcination. As shown in Fig. 1c and d, the 2D planes of HNCN collapsed significantly and generated regular nanotubes with mesopores of approximately 2.7 µm in length and 70-90 nm in diameter. Moreover, the transmission electron microscopy (TEM) image of HNCN showed preserved nanotubes after 2D planar collapse (Fig. 1e), whereas the diameter of the nanotubes was close to that observed in the scanning electron microscopy (SEM) image and exhibited a porous shape (Fig. 1f). Fig. 1g shows that HNCN exhibited single-layered tube walls, indicating a hollow interior that can facilitate the increase in specific surface area and the exposure of internal active sites [42]. Fig. 1h and i show the SEM images of the Cu-HNCN catalysts. The Cu-HNCN catalysts exhibited severe collapse after thermal polymerization and retained regular pore-rich nanotubes with diameters in the range of 70-80 nm. Additionally, the Cu, C, and N species were

uniformly distributed on the surface of the Cu-HNCN catalyst (Fig. 1j). Furthermore, TEM images of the Cu-HNCN catalyst confirmed that the catalyst had a monolayer porous tube wall (Fig. 1k and l) with a mesopore size of approximately 20-30 nm. No copper-containing nanoparticles were found on the surface of Cu-HNCN, and no lattice fringes attributable to copper oxides or copper-carbon clusters were observed in the high-resolution TEM image (Fig. 1m), indicating that neither copper oxides nor copper-carbon clusters were present in Cu-HNCN. The hollow porous properties of the nanotubes in the catalyst were further demonstrated by high-angle annular dark-field (HAADF) imaging (Fig. 1n). The HAADF-mapping images showed a high distribution and size uniformity of Cu, C, and N atoms on the Cu-HNCN surface. Meanwhile, the Cu and N atoms were distributed with uniform adjacency, suggesting the possible presence of Cu-N complexation sites [43]. By contrast, the Cu and O atoms were distributed with large spacing, which in turn proved the absence of Cu-containing oxides. The SEM and TEM images suggest that the Cu species were highly dispersed on HNCN. In addition, Cu-CN was present in the disordered 2D sheets, and the Cu species were highly dispersed (Fig. S1).

Fig. S2a shows the N2 adsorption-desorption curves of different catalysts. All samples showed an H4 hysteresis loop, indicating that abundant pores were present in the CN matrix [44]. The pore size distribution curves (Fig. S2b) showed that the HNCN and Cu-HNCN catalysts possessed large average pore sizes and pore volumes, which can be attributed to their rich pore structures. Table 1 summarizes the structural characteristics of CN, Cu-CN, HNCN, and Cu-HNCN. The Brunauer-Emmett-Teller (BET) specific surface area of HNCN reached $80.59 \text{ m}^2/\text{g}$, which is larger than that of disordered CN (59.20 m²/g). In addition, the pore volume and size of HNCN were significantly larger than those of CN $(0.594 \text{ cm}^3/\text{g} \text{ and } 29.60 \text{ nm vs. } 0.263 \text{ cm}^3/\text{g} \text{ and }$ 18.05 nm). Therefore, the large specific surface area of HNCN is consistent with its rich pore structure. Although the specific surface area, pore volume, and pore size of Cu-HNCN were slightly reduced $(73.87 \text{ m}^2/\text{g}, 0.498 \text{ cm}^3/\text{g}, \text{ and } 26.98 \text{ nm})$ because of the anchoring of Cu (the pore diameter was consistent with the results observed in the TEM image), they were significantly larger than those of Cu-CN $(54.41 \text{ m}^2/\text{g}, 0.255 \text{ cm}^3/\text{g}, \text{ and } 17.85 \text{ nm})$. These results revealed the good mesoporous properties of the Cu-HNCN catalyst, which are conducive to the exposure of active sites in the redox reaction [45]. The thermogravimetric curves of the Cu-CN and Cu-HNCN catalysts showed that their Cu contents were approximately 10.59% (Cu-CN) and 11.53% (Cu-HNCN) (Fig. S3). Inductively coupled plasma spectrometry (MS) was used to further determine the Cu content in the catalysts (Table S1).



Scheme 1. Preparation of Cu-HNCN catalyst.

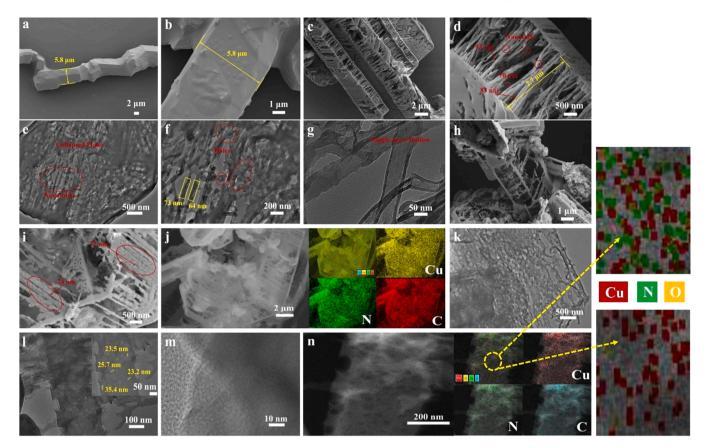


Fig. 1. SEM images of precursor: (a) 2 and (b) 1 μm. SEM images of HNCN catalyst: (c) 2 μm; (d) 500 nm. TEM images of HNCN catalyst: (e) 500, (f) 200, and (g) 50 nm. SEM images of Cu-HNCN catalyst: (h) 1 μm and (i) 500 nm. Elemental mapping images: (j) 2 μm. TEM images of Cu-HNCN catalyst: (k) 500, (l) 100, and 50 and (m) 10 nm. HAADF-scanning TEM and elemental mapping images: (n) 200 nm.

 $\begin{tabular}{ll} \textbf{Table 1} \\ \textbf{Specific surface area, pore volume, and pore diameter of different catalysts.} \\ \end{tabular}$

- 4				
	Catalysts	$S_{BET} (m^2/g)$	Total pore volume (cm ³ /g)	Pore diameter (nm)
	CN	59.20	0.263	18.05
	Cu-CN	54.41	0.255	17.85
	HNCN	80.59	0.594	29.60
	Cu-HNCN	73.87	0.498	26.98
	Cu-HNCN	/3.8/	0.498	20.98

The accurate Cu contents were 9.68 and 10.72 wt% for Cu-CN and Cu-HNCN, respectively.

The phase structure of the catalysts was determined using X-ray diffraction (XRD). As shown in Fig. 2a, the characteristic diffraction of the CN and HNCN samples at 27.3° was attributed to the interlayer stacked (002) crystalline phase of CN. The intensity of the (002) peak of HNCN was weak, which may be attributed to the size-dependence of the nanotubes [46]. In addition, the (002) characteristic diffraction of Cu-CN and Cu-HNCN slightly shifted to higher angles, and the conjugate plane spacing was reduced to 0.321 and 0.319 nm compared with the 0.329 and 0.323 nm, respectively, compared to those of CN and HNCN. Evidently, Cu doping affected the growth of CN crystals. Moreover, the intensity of the peak attributed to the (100) crystal plane at 13.2° was weaker in HNCN than in CN and almost invisible in Cu-HNCN, indicating that the nanotubes had a small planar layer size [47]. The anchor of Cu did not destroy the CN matrix phase, and no copper oxides or copper-carbon cluster diffraction peaks appeared in Cu-HNCN, indicating that none of the Cu species existed as copper oxides or copper-carbon clusters. Fourier infrared (FTIR) spectroscopy was performed to study the local chemical characteristics of the catalysts. As shown in Fig. 2b, the IR bands of Cu-CN, HNCN, and Cu-HNCN were

consistent with those of the original CN, indicating the stability of the CN matrix. However, the intensities of Cu-CN and Cu-HNCN were slightly weaker than those of CN and HNCN in the 1228 and 1314 cm $^{-1}$ bands, corresponding to N-(C3) and C=N-C vibrations, respectively, in aromatic heterocyclic compounds. This phenomenon was attributed to the coordination of the N point in CN with the Cu atom, which affected the stretching vibration of the aromatic heterocyclic ring [16,29]. Moreover, significantly enhanced absorption vibrations of HNCN and Cu-HNCN in the 3000–3500 cm $^{-1}$ band, which correspond to surface-bonded water molecules and amino groups, were observed, indicating that HNCN and Cu-HNCN have large open surfaces [48] because of the successful construction of hollow nanotubes.

The elemental composition and electronic properties of Cu-HNCN were investigated by X-ray photoelectron spectroscopy (XPS). Table S2 lists the atomic compositions of all samples. As shown in Fig. 2c, the peaks at 284.5, 286.6, and 287.9 eV in the C1 s spectrum of CN are attributed to $sp^2 \, C$ and $C\text{-}NH_x$ (x = 1, 2) at the edge of the heptazine unit and N-C=N [49]. The construction of HNCN and the anchoring of Cu caused no change in the C1 s spectrum. Several changes were observed in the N1 s spectrum (Fig. 2d). The peaks at 398.5, 399.6, and 400.9 eV in CN were attributed to N (N-C=N), N-(C₃), and NH_x (x = 1, 2), respectively [50]. By contrast, the peaks of N (N-C=N) and N-(C₃) in HNCN shifted slightly to lower binding energies, and the area of the NH_x ($x=1,\,2$) peaks was reduced. This phenomenon was attributed to the changes in bond energy between C and N atoms caused by the plane bending of HNCN [51], whereas the reduction in plane edges containing NH_x (x = 1, 2) was attributed to the construction of nanotubes. Cu-HNCN exhibits a peak at 399.3 eV, which is attributed to the coordinated nitrogen in CuN_x [52]. In addition, the peaks of N (N-C=N), N-(C₃), and NH_x (x = 1, 2) shifted to higher binding energies than those of HNCN, indicating that the appearance of Cu atoms reduced the

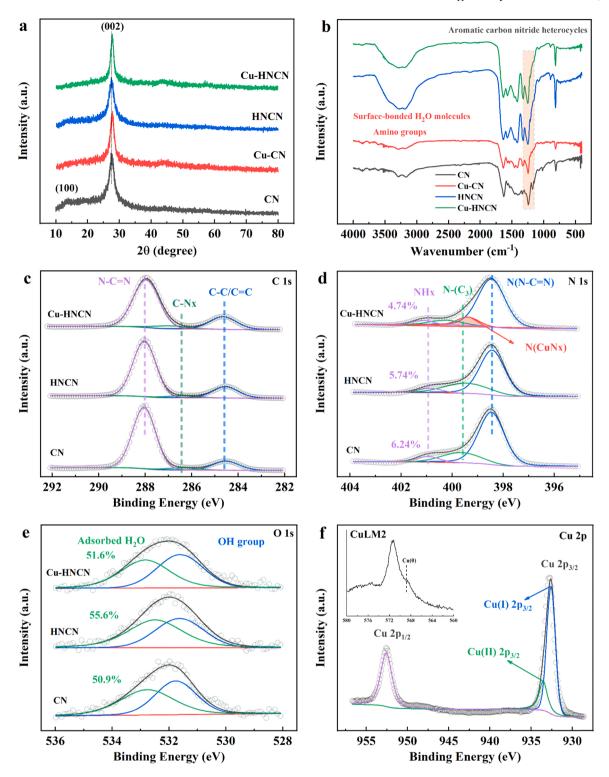


Fig. 2. (a) XRD patterns and (b) FTIR spectroscopy spectra of CN, Cu-CN, HNCN, and Cu-HNCN. XPS of (c) C 1s, (d) N 1s, and (e) O 1s spectra of CN, HNCN, and Cu-HNCN. (f) Cu 2p spectrum and Cu LM2 Auger spectrum (inset) of Cu-HNCN.

electron density of N atoms, resulting from the formation of Cu-N coordination bonds [16]. Notably, the surface content of CuN_X increased with increasing Cu doping from 6.97% for 1Cu-HNCN to 13.62% for 4Cu-HNCN (Fig. S4). Thus, given the high nitrogen content in the CN matrix, Cu species can be firmly bound to the nitrogen ligand [21,53]. Furthermore, the O 1 s spectra of the three catalysts showed the same O species (Fig. 2e) with binding energies of 531.8 and 532.9 eV, which were attributed to surface O-H and adsorbed H_2O , respectively [54].

HNCN and Cu-HNCN exhibited high contents of adsorbed $\rm H_2O$, which was attributed to the expanded specific surface area due to the nanotubular morphology. As shown in Fig. 2f, the peaks at 932.3 and 933.5 eV in the Cu 2p spectrum were attributed to $\rm 2p_{3/2}$ Cu(I) and Cu (II), respectively. The presence of Cu(I) was attributed to the production of reduced NH₃ during thermal polymerization. Moreover, no Cu(0) peak was found in the Cu LM2 Auger spectrum (inset of Fig. 2f), implying that all the Cu in Cu-HNCN was present as

single-electron-capacity CuN_{x} redox sites. Therefore, all the characterization results demonstrate that highly diffuse CuN_{x} sites were successfully incorporated into Cu-HNCN.

3.1.2. Photogenerated charge separation and transfer analysis

The optical absorption and charge separation/transfer behaviors of all samples were systematically studied. As shown in Fig. 3a, the light absorption edge of HNCN red-shifted, and the absorption intensity in the visible-light region increased compared with that of disordered CN, indicating that the nanotubular structure improved visible-light utilization. This finding can be attributed to the reflection of incident light in the tube, which improved light absorption [55] and can be explained by

quantum confinement effects. According to the particle-in-a-box approximation, the thinner the low-dimensional material, the stronger its confinement effect [51]. The strengthened confinement effect caused by the single-layer tube wall of HNCN can cause differences in the bandgap. Furthermore, the visible-light absorption of the Cu-CN and Cu-HNCN catalysts was significantly enhanced, which may be attributed to metal doping narrowing the bandgap of the materials. The band gap energies of Cu, Cu-CN, HNCN, and Cu-HNCN calculated using the Kubelka–Munk formula were 2.87, 2.62, 2.81, and 2.54 eV, respectively (Fig. 3b). Thus, the construction of nanotubes and the anchoring of CuN $_{\rm X}$ sites narrowed the bandgap energy of Cu-HNCN, which in turn enhanced its visible-light utilization [56]. In addition, the edge potential of

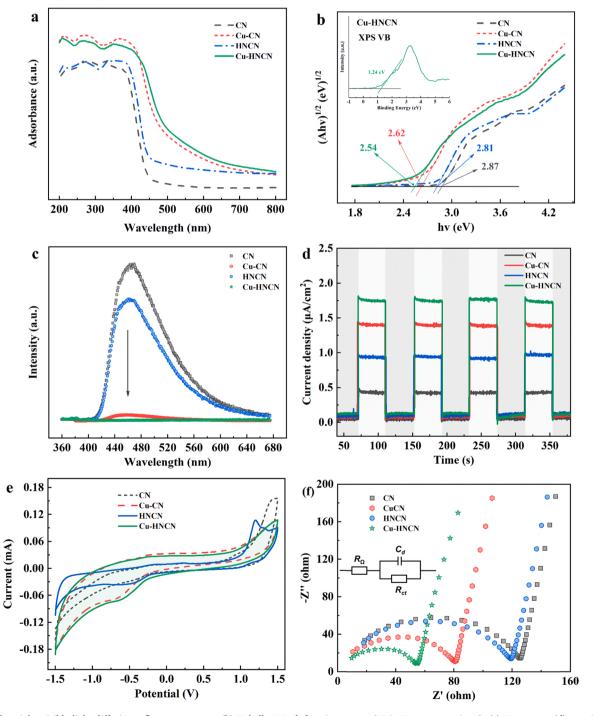


Fig. 3. (a) Ultraviolet-visible light diffusion reflectance spectra, (b) Kubelka–Munk function curves (XPS; VB spectrum, inset), (c) PL spectra, (d) transient photocurrent, (e) CV curves, and (f) Nyquist plots of CN, Cu-CN, HNCN, and Cu-HNCN.

Cu-HNCN was obtained from the XPS valence-band spectra (Fig. 3b, inset). The calculated E_{VB} was 1.24 eV, whereas the E_{CB} was -1.30 eV according to Eq. (2), indicating that O_2 can generate O_2 from the CB of Cu-HNCN during photocatalysis $(O_2/O_2: -0.33 \text{ eV})$, whereas H_2O cannot generate OH directly from the VB $(H_2O/OH: 2.40 \text{ eV})$ [25,57].

$$E_g = E_{VB} + E_{CB} \tag{2}$$

Photoluminescence (PL) spectroscopy, photocurrent response, cyclic voltammetry (CV) curves, and electrochemical impedance spectroscopy (EIS) were used to investigate the charge separation/transport performance of the Cu-HNCN catalysts in detail. First, the original CN exhibited a distinct photocarrier recombination signal at 470 nm (Fig. 3c) [58]. The recombination signal of Cu-CN was significantly quenched, indicating that the presence of CuNx sites inhibited the recombination of photogenerated charges. The charge recombination signal of HNCN was also suppressed compared to that of CN, and Cu-HNCN was detected with an almost completely quenched PL signal. indicating the best photogenerated charge separation performance. Fig. 3d shows the transient photocurrent response of the prepared catalysts under dark/light illumination. Cu-CN exhibited a stronger photocurrent signal than CN because of the capture of electrons by Cu (II)Nx, which facilitated the separation and transfer efficiency of photogenerated charges [59]. Moreover, Cu-HNCN exhibited the strongest photocurrent signal, indicating that the nanotubes promoted charge separation. Similar results were obtained for the CV curves and EIS analyses. As shown in Fig. 3e, Cu-HNCN exhibited the largest CV ring area, revealing its excellent charge-transfer capability. As shown in Fig. 3f, the high-frequency regions of the Nyquist plots for all four samples show semicircles, which indicate the ohmic resistance and charge transfer impedance of the electrode–electrolyte interface [60]. Particularly, HNCN had a smaller Nyquist arc radius than CN, indicating that the nanotubes reduced the charge-transfer resistance. Cu-CN also showed a small Nyquist arc radius, indicating that the CuNx sites improved charge transfer and conductivity. Importantly, Cu-HNCN exhibited the smallest Nyquist arc radius in the high-frequency region, indicating its excellent charge transfer and transport capabilities.

The above results prove that the anchoring of CuN_x sites and the construction of nanotubes contributed to the separation and transfer of photogenerated charges. First, the $\text{Cu}(\text{II})\text{N}_x$ in the CuN_x site can capture electrons and be reduced to $\text{Cu}(\text{II})\text{N}_x$, which realizes effective charge separation [29,61]. Second, according to the quantum confinement effect, the reduction of the dimensionality of the semiconductor material can enhance quantization along the confinement direction, implying a large difference in the density of states in the length and diameter directions of the nanotube [62]. These differences result in a high tendency for carriers to migrate along the length of the nanotube; this migration is more efficient than disordered migration in the 2D plane of pristine CN [63]. Thus, the unique nanotube-like structure of Cu-HNCN may achieve the directional migration of electrons, which in turn enhances charge separation and transport.

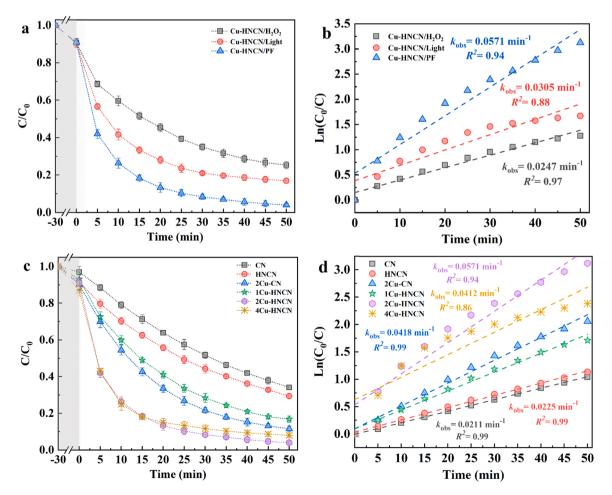


Fig. 4. (a) TET degradation with Cu-HNCN through different reaction systems. (b) Kinetics of TET degradation with Cu-HNCN through different reaction systems. (c) TET degradation with different catalysts through PF system (20 °C, catalyst dosage = 0.2 g/L, H_2O_2 concentration = 20 mM, pH = 6.5, TET = 10 mg/L).

3.2. PF degradation performance

3.2.1. Effect of different systems

As shown in Fig. S5, TET barely degraded under H2O2, light, and H₂O₂/light without a catalyst, indicating that the homogeneous system alone cannot degrade TET. Fig. 4a shows the degradation performance of Cu-HNCN on TET in different systems. Cu-HNCN can degrade TET in the presence of H₂O₂, and the degradation efficiency reached 74.7% within 50 min, indicating that the CuNx sites in Cu-HNCN activated H₂O₂ [16]. Under visible-light illumination, the degradation efficiency of Cu-HNCN for TET reached 83.0% within 50 min, suggesting the visible photocatalytic activity of Cu-HNCN. Notably, the TET degradation efficiency of the Cu-HNCN/PF system reached 96.0% within 50 min, with a fitted first-order kinetic rate constant (k_{obs}) of 0.0571 min⁻¹ (Fig. 4b), which was higher than those of the $Cu-HNCN/H_2O_2$ (0.0247 min⁻¹) and Cu-HNCN/light (0.0305 min⁻¹) systems by 2.3 and 1.9 times, respectively. The excellent TET degradation performance indicated that the Cu-HNCN/PF system had good catalytic activity, which may be attributed to the intrinsic promotion mechanism of the heterogeneous Fenton-like and photocatalytic reactions [29,64]. Briefly, the Cu-HNCN catalyst was excited by visible light to generate photogenerated electrons, and owing to its excellent charge separation and transport properties, the reuse of Cu(I)Nx and activation of H2O2 were enhanced.

Fig. 4c shows the TET degradation by the different catalysts during the PF reaction. The TET degradation efficiency of CN after 50 min was 65.9%, whereas HNCN showed higher catalytic activity with a 70.7% degradation efficiency. This result was attributed to the enlarged specific surface area and rich pore structure of HNCN, which increased the number of catalytically active sites. In addition, photoelectrochemical tests proved that HNCN possesses strong photoelectrochemical properties, which also contribute to the degradation of TET [65]. Notably, 2Cu-CN and 2Cu-HNCN with an initial Cu content of 2% exhibited enhanced TET degradation, with degradation efficiencies of 88.5% and 96.0% within 50 min, respectively. The anchoring of copper species significantly promoted TET degradation, indicating the important role of the CuN_x active sites in activating H₂O₂ during the PF process [29]. In addition, with a similar Cu content, the $k_{\rm obs}$ values of Cu-HNCN were significantly higher than those of Cu-CN (0.0571 min⁻¹ 0.0418 min⁻¹) (Fig. 4d), suggesting the role of hollow nanotubes, including the provision of a larger specific surface area, richer pores, stronger light absorption, and more efficient charge separation/transport [66]. The TET degradation efficiencies of Cu-HNCN with different Cu contents during PF were in the order 2Cu-HNCN (96.0%) > 4Cu-HNCN (92.0%) > 1Cu-HNCN (83.3%), and the corresponding $k_{\rm obs}$ were in the order 2Cu-HNCN (0.0571 min⁻¹) > 4Cu-HNCN $(0.0412 \text{ min}^{-1}) > 1\text{Cu-HNCN} \ (0.0346 \text{ min}^{-1})$. Thus, the 2Cu-HNCN catalyst was used in subsequent experiments.

3.2.2. Effect of H_2O_2 concentration, catalyst dosage, initial pH, TET concentration, coexisting substances, and water matrix

The effects of the $\rm H_2O_2$ concentration, catalyst dosage, initial pH, coexisting substances, and water matrix on the degradation of TET by the Cu-HNCN/PF system were investigated to study the intrinsic linkage and applicability of the system. As shown in Fig. S6a, when the $\rm H_2O_2$ concentration increased from 2.0 mM to 20 mM, the TET degradation efficiency increased from 88.4% to 96.0%, and $k_{\rm obs}$ increased from 0.0352 min⁻¹ to 0.0571 min⁻¹. When the $\rm H_2O_2$ concentration was further increased to 30 mM, the TET degradation performance showed no significant enhancement (96.7% TET degradation efficiency and 0.0627 min⁻¹ $k_{\rm obs}$). An appropriate increase in the $\rm H_2O_2$ concentration can increase the OH concentration, which in turn accelerates the degradation. However, excessive $\rm H_2O_2$ can cause oversaturation of the reaction sites and result in the scavenging of OH, which can inhibit degradation [67].

Fig. S6b shows the effect of the catalyst dosage. The dosage of Cu-

HNCN increased from $0.05 \, \mathrm{g/L}$ to $0.2 \, \mathrm{g/L}$, corresponding to an increase in TET degradation efficiency from 87.4% to 96.0% and k_{obs} from $0.0359 \, \mathrm{min}^{-1}$ to $0.0571 \, \mathrm{min}^{-1}$. However, when the catalyst dosage was increased to $0.4 \, \mathrm{g/L}$, the degradation efficiency did not increase accordingly (95.4%), and the corresponding k_{obs} was suppressed (0.0529 min^{-1}). TET degradation was positively correlated with catalyst dosage over a certain range, confirming the role of heterogeneous reactions. Excess catalyst in the aqueous phase agglomerates and may affect the transmission of visible light, thereby affecting the PF process.

Fig. S6c shows the effect of the TET concentration. The removal efficiencies at TET concentrations of 5, 10, 20, and 40 mg/L were 97.2%, 96.0%, 94.6%, and 90.1%, respectively. The TET removal efficiency decreased with increasing TET concentrations. The number of active species produced in the system was approximately constant for the same operating parameters. Therefore, more active species are required for the degradation of high concentrations of pollutants.

Fig. 5a shows the effect of different initial pH values on TET degradation. The pH of the TET solution without HCl or NaOH treatment is 6.5. Overall, the TET degradation efficiencies at pH = 6.5, 3, 4, 5, 6, 7, 89 were 96.0%, 68.3%, 92.4%, 95.4%, 96.1%, 94.9%, 88.9%, and 71.6%, respectively, corresponding to k_{obs} of 0.0571, 0.0226, 0.0503, 0.0570, $0.0552\ 0.0522,\ 0.0382,\ and\ 0.0206\ min^{-1}$. The degradation of TET at pH = 3 was severely inhibited, and this was attributed to the introduction of Cl by HCl, which in turn scavenged OH to produce the less oxidizable·ClOH [68]. By contrast, the TET degradation efficiency was significantly higher at pH = 4. Therefore, the weak TET degradation under strong acidity was not solely due to the quenching effect of Cl-. The zero-point charge of Cu-HNCN measured using the zeta potentiometer was 4.3 (Fig. S7), indicating positive and negative potentials on the catalyst surface at pH < 4.3 and pH > 4.3, respectively. Meanwhile, TET is mainly present as TCH³⁺ at pH < 3.3 and as TCH⁻ and TC²⁻ at pH > 7.7 [3]. Thus, the electrostatic repulsion between the catalyst surface and TCH3+ under strong acidity also inhibits TET degradation. In addition, electrostatic repulsion exists under alkaline conditions, and the additional decomposition of H₂O₂ can inhibit the PF process [69].

Fig. 5b shows the effect of inorganic anions (including Cl⁻, NO₃⁻, CO₃²⁻, HPO₄²⁻, and SO₄²⁻) on the degradation of TET. At a Cl⁻ concentration of 20 mM, the TET degradation efficiency was reduced to 88.1%, which was attributed to the low oxidation capacities of ClOH and Cl-. The presence of NO₃ had a negligible effect (92.9% degradation efficiency in 50 min) owing to the generation of the NO3 oxidant [70]. The inhibitory effect was significant in the presence of CO₃², and the degradation efficiency of TET decreased to 79.7% at a concentration of 20 mM. CO_3^{2-} can produce HCO_3^{-} and H_2CO_3 in water to increase the pH of the reaction solution and act as scavengers of OH [71]. HPO₄²⁻ also exhibited an inhibitory effect, and the degradation efficiency of TET at 20 mM decreased to 80.3%, which was attributed to the formation of HPO4·with·OH or the increase in solution pH. Remarkably, the TET degradation efficiency was not inhibited in the presence of SO₄²-, reaching 96.3% at 20 mM SO₄²-owing to the generation of the strong oxidant SO₄² [72]. Humic acid was selected as typical natural organic matter (NOM) to investigate the effect of NOM on the degradation process. As shown in Fig. 5c, when the HA concentration increased from 3 to 10 mg/L, the degradation efficiency decreased from 89.9% to 82.5%, and $k_{\rm obs}$ decreased from 0.0381 min⁻¹ to 0.0286 min⁻¹. The addition of HA inhibited the degradation of TET owing to the additional consumption of radicals by HA. Moreover, the phenolic hydroxyl and carboxyl groups of HA could be adsorbed on the Cu-HNCN surface, shielding the reaction sites.

The degradation of TET by the Cu-HNCN/PF system in real water bodies was investigated using River A and Lake B as the water matrix (Fig. 5d); the chemical oxygen demand (COD), total nitrogen (TN), and total phosphorus (TP) of River A were lower than those of Lake B, which was attributed to the improved self-purification capability of flowing water bodies [73]. Compared with the ultrapure water matrix, the TET degradation efficiency in River A and Lake B declined to 89.2% and

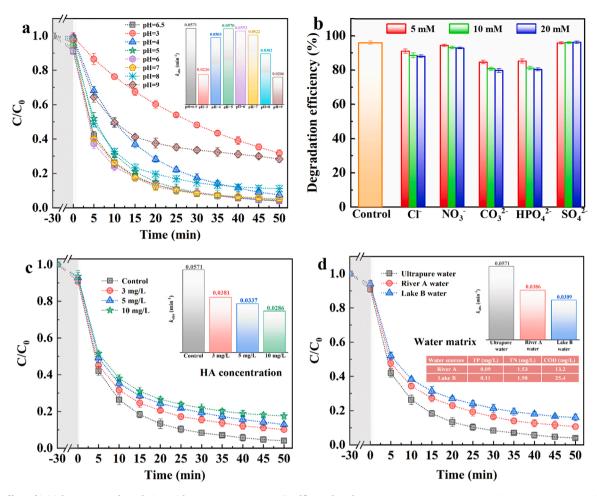


Fig. 5. (a) Effect of initial pH on TET degradation with Cu-HNCN/PF system (20 °C, catalyst dosage =0.2 g/L, H_2O_2 concentration =20 mM, TET =10 mg/L). (b) Effect of inorganic ions on TET degradation with Cu-HNCN/PF system (20 °C, catalyst dosage =0.2 g/L, H_2O_2 concentration =20 mM, TET =10 mg/L). (c) Effect of NOM on TET degradation with Cu-HNCN/PF system (20 °C, catalyst dosage =0.2 g/L, H_2O_2 concentration =20 mM, pH =6.5, TET =10 mg/L). (d) Effect of different water sources on TET degradation with Cu-HNCN/PF system (20 °C, catalyst dosage =0.2 g/L, H_2O_2 concentration =20 mM, TET =10 mg/L).

84.2%, respectively. The degradation of TET was influenced by the real water matrix, which was closely related to the presence of anions, NOM, and bacteria in real water bodies. These components compete with pollutants for active sites and radicals. Overall, the Cu-HNCN/PF system maintained the TET degradation capacity (more than 80% degradation efficiency) in real complex water bodies. Table S3 summarizes the reported degradation of TET via photocatalytic and Fenton-like reactions. The Cu-HNCN-mediated PF process demonstrated stronger TET removal and faster catalytic reaction rate than the photocatalytic and Fenton-like processes with a lower catalyst dosage, revealing the advantage of the Cu-HNCN/PF system for TET degradation.

3.3. Geometric optimization and DFT calculation

Atomic models of planar Cu-CN and nanotube Cu-HNCN were developed and their structures were optimized. As shown in Fig. 6a and b, the bond lengths and angles of the geometrically optimized nanotube atomic models changed to reach the most stable state. Compared with the planar model, the bond lengths between the C and N atoms in the nanotubes appeared different, and the change in bond length led to a change in bond energy, which is consistent with the XPS results. Emphatically, compared with 2.13–2.22 Å in the planar model, the Cu-N bond length in the nanotubes was significantly shortened to 1.93–1.96 Å due to the bending of the planes. In general, short Cu-N bonds exhibit strong interactions and high bond energies, which may stabilize Cu in Cu-HNCN [74].

The differential charge density was calculated to investigate the effect of nanotubes on charge transport. As shown in Fig. 6c, the yellow region represents charge enrichment, and the blue region represents charge depletion. The nanotube atom model demonstrated high density and large areas of charge enrichment and depletion, suggesting that the model was beneficial for charge separation and transport [23]. Therefore, the differential charge density calculation results confirmed that Cu-HNCN exhibited enhanced charge separation and transport performance compared to planar Cu-CN. In addition, a large region of charge depletion around the Cu atom was observed in the nanotube model. The short Cu-N bond length caused by the nanotubes means that the electronegativity difference between Cu and N atoms increases, resulting in a large attraction difference between Cu and N for electrons, which could increase the tendency of electron enrichment in the Cu-adjacent N atoms.

3.4. Stability study

The reusability of the Cu-HNCN and Cu-CN catalysts was investigated (Fig. 7a). After 10 cycles of reuse, the TET degradation efficiencies of Cu-HNCN and Cu-CN in the PF process decreased from 96.0% and 88.5–82.9% and 68.7%, respectively. The decrease in the degradation efficiency was attributed to the shielding of the active sites by the intermediates. The catalytic activity was reset after the catalysts were fully washed, dried, and annealed at 550 °C for 1 h. The TET degradation efficiencies of the recovered Cu-HNCN and Cu-CN catalysts declined

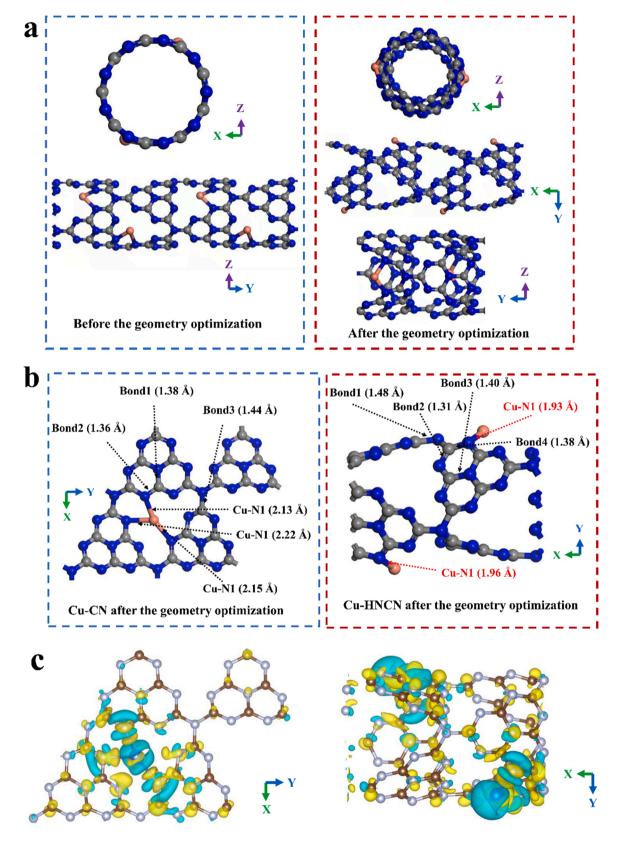


Fig. 6. (a) Atomic model of the Cu-HNCN before and after geometric optimization. (b) Atomic model of Cu-CN and Cu-HNCN after geometric optimization and the corresponding bond length. (c) Calculated charge density difference of Cu-CN and Cu-HNCN (the yellow and cyan areas indicate charge accumulation and depletion, respectively).

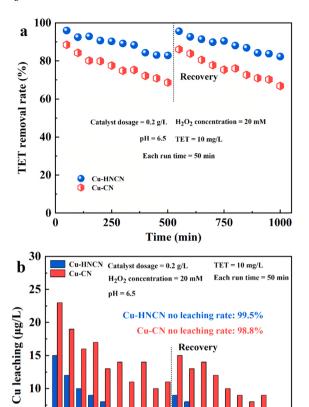


Fig. 7. (a) TET removal by Cu-HNCN and Cu-CN under PF reaction in 20 cycles (20 °C, catalyst dosage =0.2 g/L, $\rm H_2O_2$ concentration =20 mM, pH =6.5, TET =10 mg/L). (b) Cu leaching amounts of Cu-HNCN and Cu-CN in each cycle (20 °C, catalyst dosage =0.2 g/L, $\rm H_2O_2$ concentration =20 mM, pH =6.5, TET =10 mg/L).

500

Time (min)

750

250

from 95.6% and 86.1–82.3% and 66.9%, respectively, over 10 cycles. Cu-HNCN showed slight inhibition of TET degradation, which could be related to the stable CuN_x sites. The Cu concentration remaining in the solution with Cu-HNCN was significantly lower than that of Cu-CN (Fig. 7b), and the Cu retention of Cu-HNCN after 20 cycles was 99.5%. The short Cu-N bonds (1.93–1.96 Å) of Cu-HNCN obtained from DFT calculations further stabilized the catalyst, revealing that nanotubes can improve catalyst stability.

Furthermore, the XRD patterns showed that the (002) crystal plane of Cu-HNCN exhibited a good characteristic diffraction after cycling (Fig. S8a), indicating that Cu-HNCN can maintain its structural stability during long-term operation. The retained Cu-HNCN nanotubes were confirmed by SEM images (Fig. S8b and c). Fig. S8d shows the Cu 2p spectra of the fresh and recycled catalysts. The $2p_{3/2}$ Cu(I)/ $2p_{3/2}$ Cu(II) content in Cu-HNCN before and after use decreased slightly from 79.75/20.25 to 77.23/22.77. The valence state of Cu was maintained owing to the excellent photogenerated charge separation and transport performance of Cu-HNCN, which allowed the effective reduction of Cu(I) after the activation of H_2O_2 to form Cu(II). The above results further indicate that Cu-HNCN possesses good stability, which provides a reference for the application of this catalyst in complex water purification.

3.5. Mechanism of PF degradation

3.5.1. Identification of radical species

As a typical free radical in Fenton-like reactions, OH has been studied for the first time. Isopropyl alcohol (IPA) was used as an OH scavenger, and the results are shown in Fig. 8a. When the IPA concentration increased from 5 mM to 100 mM, the TET degradation efficiency decreased from 89.8% to 84.7%, indicating that OH was an important radical for TET degradation. Benzoquinone (BQ) was used as a quencher for O2 to investigate the role of O2 in the PF process. As shown in Fig. 8b, the degradation efficiency of TET declined from 91.6% to 74.1% when the BQ concentration was increased from 0.05 mM to 0.2 mM. The TET degradation was significantly inhibited by the scavenging of O₂, proving that O₂ was the dominant radical in the Cu-HNCN/PF system. The contribution of h+ ions to the degradation of TET was also investigated. As shown in Fig. 8c, when the concentration of triethanolamine (TEOA) increased from 25 mM to 100 mM, the TET degradation efficiency decreased from 88.5% to 82.4%. In addition, the roles of electron and non-radical ROS were probed using AgNO3 and histidine (L-His) as electron and ¹O₂ scavengers, respectively (Fig. 8d and e). The efficiency of TET degradation after complete quenching of electrons and ¹O₂ decreased to 91.9% and 89.2%, respectively. The results of quenching experiments showed that OH, O₂, h⁺, e⁻, and ¹O₂ played a role in TET degradation. Fig. 8f summarizes the inhibition of $k_{\rm obs}$ in the Cu-HNCN/ PF system by quenching all radicals and non-radical ROS. The results showed that the main free species responsible for TET degradation were O_2^- and h^+ (inhibition of k_{obs} reached 64.1% and 48.7%, respectively) and that OH also played an important role (inhibition of k_{obs} was 45.3%). Notably, ${}^{1}O_{2}$ inhibited k_{obs} by 31.1%, suggesting that it was a non-radical ROS for TET degradation.

The dominant role of O_2 and h^+ in the PF reaction was attributed to the excellent visible-light utilization and capability to separate photogenerated electron-hole pairs in the Cu-HNCN catalyst [11,75]. The CB of Cu-HNCN accumulated large numbers of photogenerated electrons, which in turn reacted with O_2 on the catalyst surface to form O_2 (as demonstrated in Section 3.1.2) (Eqs. (3–4)). Electrons were fully consumed owing to the generation of O_2 and participation in the valence cycle of Cu(I/II) (Eqs. (4–5)). Thus, the h^+ of the VB of Cu-HNCN was released to participate in TET degradation. The important role of OH was attributed to the efficient activation of H_2O_2 by the Cu-HNCN catalyst (Eqs. (6–7)). In addition, 1O_2 production was due to the reaction of abundant O_2 in the system with H^+ , H_2O_2 , and OH (Eqs. (8–10)) [76].

Cu-HNCN + Visible Light
$$\rightarrow e^{-}(CB) + h^{+}(VB)$$
 (3)

$$e^{-}(CB) + O_2 \rightarrow O_2^{-}$$
 (4)

$$Cu(II)N_x + e^- \rightarrow Cu(I)N_x$$
 (5)

$$Cu(I)N_x + H_2O_2 \rightarrow Cu(II)N_x + OH + OH^-$$
(6)

$$Cu(II)N_x + H_2O_2 \rightarrow Cu(I)N_x + HO_2 + H^+$$
(7)

$$\cdot O_2^- + \cdot O_2^- + 2H^+ \rightarrow {}^1O_2 + H_2O_2$$
 (8)

$$\cdot O_2^- + \cdot O_2^- + H_2O \rightarrow 1.5^1O_2 + 2OH^-$$
 (9)

$$\cdot O_2^- + \cdot OH \rightarrow {}^1O_2 + OH^-$$
 (10)

The production of OH was semi-estimated by electron paramagnetic resonance (EPR) using DMPO as a trapping agent. As shown in Fig. 9a, Cu-HNCN and Cu-CN had four distinctive 1:2:2:1 characteristic peaks of DMPO-OH adducts during the PF reaction [77], indicating that $\rm H_2O_2$ was activated by the copper species. In particular, the stronger signal intensity of DMPO-OH in the Cu-HNCN/PF system suggests that $\rm H_2O_2$ was effectively activated by Cu-HNCN, proving the positive role of nanotubes in TET degradation. The generation of OH from Cu-HNCN in the different reaction systems was also compared. As shown in Fig. 9b, Cu-HNCN/PF exhibited a more pronounced DMPO-OH signal than the

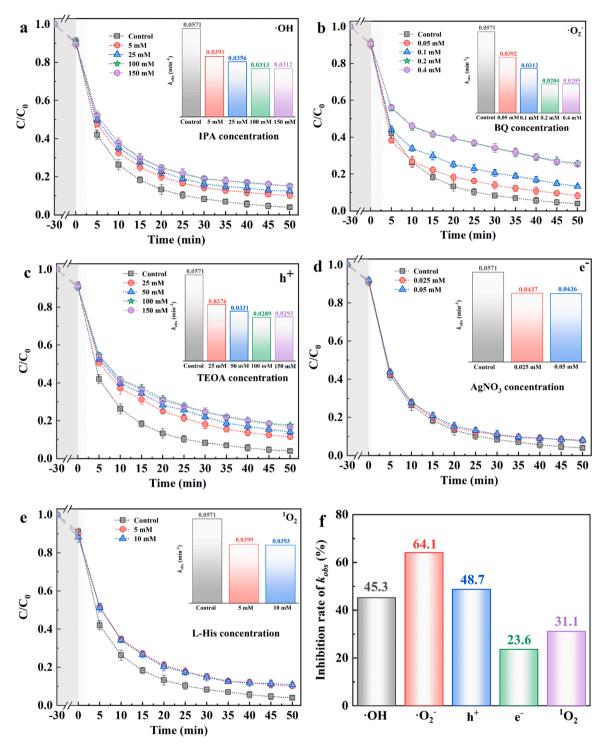


Fig. 8. (a) Effect of radical scavengers on TET degradation with Cu-HNCN/PF system: (a) IPA, (b) BQ, (c) TEOA, (d) AgNO₃, and © L-His (20 °C, catalyst dosage = 0.2 g/L, $\rm H_2O_2$ concentration = 20 mM, pH = 6.5, TET = 10 mg/L). (f) Inhibition rate of $k_{\rm obs}$ by different radicals (Inhibition rate of $k_{\rm obs}$ (%) = 1- $k_{\rm obs}/k_{\rm obs0}$).

Cu-HNCN/ H_2O_2 system, indicating that visible light promoted the activation of H_2O_2 . Further, the decomposition efficiency of H_2O_2 was investigated. As shown in Fig. S9, the decomposition efficiency of H_2O_2 in Cu-HNCN/PF reached 85.7% within 50 min, which was higher than those of the Cu-CN/PF (71.1%) and Cu-HNCN/ H_2O_2 (62.4%) systems. The decomposition of H_2O_2 is directly related to the amount of OH in the system; thus, the Cu-HNCN/PF system demonstrated enhanced H_2O_2 activation capacity [78]. This result indicates that the nanotubes and visible-light illumination enhanced the activation of H_2O_2 . The efficient

charge separation/transport of nanotubes under visible light can promote Cu(I) regeneration and H_2O_2 activation (Eqs. (5–6)).

In addition, the generation of O_2 and 1O_2 in the Cu-HNCN/PF and Cu-CN/PF systems was detected. As shown in Fig. 9c and d, quadruplet 1:1:1:1 DMPO- O_2 and triplet 1:1:1 TEMP- 1O_2 adduct signals appeared, demonstrating the presence of both in the PF process [79]. Moreover, the stronger adduct signal in Cu-HNCN/PF indicates that Cu-HNCN produced higher concentrations of O_2 and 1O_2 . The enhanced visible-light absorption and charge separation properties of Cu-HNCN

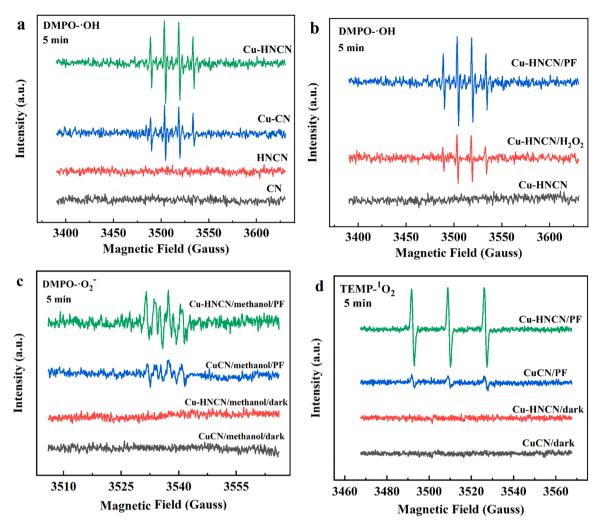


Fig. 9. (a) EPR spectra of DMPO-·OH in the PF reaction with different catalysts (20 °C, catalyst dosage = 0.2 g/L, H_2O_2 concentration = 20 mM, pH = 6.5, TET = 10 mg/L). (b) EPR spectra of DMPO-·OH obtained using Cu-HNCN with different systems (20 °C, catalyst dosage = 0.2 g/L, H_2O_2 concentration = 20 mM, pH = 6.5, TET = 10 mg/L). EPR spectra for (c) DMPO-·O₂ and (d) TEMP- 1O_2 in the PF reaction with different catalysts (20 °C, catalyst dosage = 0.2 g/L, H_2O_2 concentration = 20 mM).

can release more photogenerated electrons to generate O_2 (Eqs. (3) and (4)), whereas the more abundant O_2 can be accompanied by the generation of more 1O_2 (Eqs. (8–10)).

3.5.2. Mechanism of Cu-HNCN/PF system

The $k_{\rm obs}$ inhibition by Cu-HNCN/light and Cu-HNCN/H₂O₂ compared with that of the Cu-HNCN/PF system was calculated. Fig. S10 exhibits that the inhibition values of $k_{\rm obs}$ for TET degradation were 46.6% and 56.7% for the Cu-HNCN/light and Cu-HNCN/H₂O₂ systems, respectively, suggesting that the photocatalytic system had faster TET removal efficiency than the Fenton-like system in the presence of H₂O₂ only. This result indicates that nanotube morphology is crucial for the removal of pollutants, particularly for the enhancement of the photocatalytic activity of the PF system.

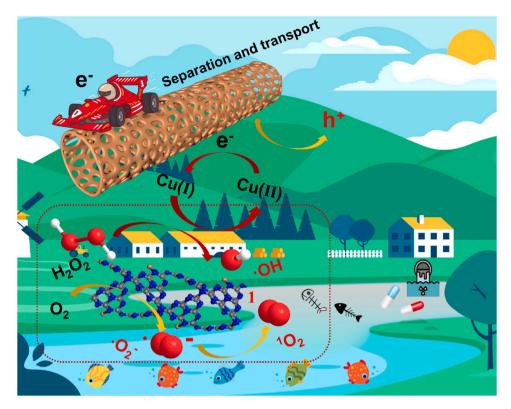
Based on the above discussion, the mechanism of TET degradation by the Cu-HNCN/PF system is summarized in Scheme 2. First, nanotube construction can enhance visible-light utilization, charge separation, and transport, whereas the additional generated and separated photogenerated electrons can react with $\rm O_2$ to form $\rm O_2$ and concomitantly produce $\rm ^1O_2$. Second, photogenerated electrons are generated and transported to achieve the effective reuse of Cu(I), which in turn enhances the activation of $\rm H_2O_2$ to produce OH. Moreover, the electrons are effectively separated and utilized to release a large amount of $\rm h^+$. Additionally, the expanded specific surface area and highly exposed

active sites of the nanotubes promoted redox reactions. Ultimately, the abundance of active species ($\cdot O_2$, $\cdot OH$, h^+ , and 1O_2) in the system and nanotube properties enable efficient degradation of TET.

Fig. S11 shows the changes in the total organic carbon (TOC) content during TET degradation. The TOC removal rate of Cu-HNCN/PF reached 60.2% within 50 min, suggesting that TET was effectively mineralized. Ofloxacin and norfloxacin were used as model contaminants to examine the oxidative selectivity of the Cu-HNCN/PF system. As shown in Fig. S12, the Cu-HNCN/PF system achieved 89.7% and 86.7% removal of ofloxacin and norfloxacin, respectively, within 50 min, while the mineralization rates were 42.1% and 37.4%, respectively, indicating that the Cu-HNCN/PF system has the potential to degrade refractory organic pollutants without selectivity. Importantly, the Cu-HNCN catalyst demonstrated better catalytic activity, especially with a faster reaction rate (0.0571 min $^{-1}$ $k_{\rm obs}$), at a lower $\rm H_2O_2$ dosage than other previously reported PF systems (Table S4), revealing the superiority of the Cu-HNCN catalyst for the removal of persistent organic pollutants.

3.6. Degradation pathways analysis

The oxidative degradation behavior of TET was predicted using the FED theory. Fig. 10a–c show the optimized TET molecular conformations and FEDs of TET with the highest occupied molecular orbital (HOMO) and lowest unoccupied molecular orbital (LUMO). Fig. 10d



Scheme 2. Proposed TET degradation mechanism by the Cu-HNCN/PF system.

shows the details of these calculations. In general, atoms with high ${\rm FED}^2_{\rm HOMO}$ values are electronically extracted during electrophilic reactions, whereas those with high ${\rm FED}^2_{\rm HOMO} + {\rm FED}^2_{\rm LUMO}$ values are susceptible to ROS attack [80]. Notably, 10(C), 12(C), 13(C), 14(C), and 27(O) exhibited high ${\rm FED}^2_{\rm HOMO}$ values, indicating that benzene rings containing 10(C), 12(C), 13(C), 14(C), and -OH, including 27(O), can be oxidized by h⁺. Moreover, high values of ${\rm FED}^2_{\rm HOMO} + {\rm FED}^2_{\rm LUMO}$ were observed for 1(C), 2(C), 3(C), 23(O), and 29(O), indicating that -C₁-C₂ = , -C₂ = C₃-, -C₁ = O₂₃, and C₃-O₂₉H are easily attacked by O₂-, OH, and 1 O₂.

Fig. S13 shows the LC-MS spectra of the intermediates during TET degradation, and Table S5 summarizes the mass-charge (m/z) signals of all intermediates. Thus, a possible TET degradation pathway can be proposed based on the FED calculation and the m/z signal. According to pathway I, the benzene ring in TET containing 10(C), 12(C), 13(C), and 14(C) atoms was first oxidized by h⁺, and the ring opened to produce A (m/z = 378). C₃-O₂₉H, an amide group, and N-methyl were further attacked by O_2 , OH, and 1O_2 to produce B (m/z = 305). C (m/z = 278) and D (m/z = 196) were obtained by demethylation, dehydration, and ring-opening. In pathway II, -C1 =O23 and C3-O29H were attacked by free species, and E (m/z = 359) and F (m/z = 314) were generated through de-N-methyl and dehydration. Then, under the attack of O_2 , OH, and ${}^{1}O_{2}$, ${}^{1}C_{2} =$ and ${}^{1}C_{2} =$ C₃- belonging to the benzene ring were oxidatively ring open to form G (m/z = 258) and H (m/z = 204), respectively. In pathway III, TET was converted to I (m/z = 460) by the addition of a hydroxyl group and then converted to J (m/z = 415) based on hydroxylation, de-N-methylation, and dehydration [81]. K (m/z = 326) was obtained via deamidation, hydroxylation, and dehydration. The benzene rings, including 10(C), 12(C), 13(C), 14(C), and -C₁-C₂ = , -C₂ =C₃- were oxidized by h^+ and O_2^- /-OH/ 1O_2 , and the ring opened to form L (m/z = 220). Finally, all intermediates, such as CO₂ and H2O, are further mineralized into smaller molecules.

In addition, the toxicity of the intermediates in the TET degradation process needs to be monitored to exclude environmental risks. Respirometry can provide sensitive and direct access to the toxicity of

contaminants in activated sludge [82]. According to the results of microbial respiration inhibition experiments (Fig. S14), the oxygen uptake of Control 2 reached 257.64 mg/L after 24 h of incubation, whereas the original TET solution significantly inhibited the respiration of activated sludge, with an oxygen uptake of 36.83 mg/L. The oxygen uptake of the Cu-HNCN/PF system-treated TET solution increased to 157.32 mg/L, indicating that the biotoxicity of the TET was reduced by the Cu-HNCN/PF system. The calculated bio-inhibition coefficient (I_r) values of 0.88 and 0.39 for the TET and treated TET groups, respectively, indicated that the biotoxicity of TET treated with Cu-HNCN/PF system was reduced by 56%, thus demonstrating that the Cu-HNCN/PF system can effectively reduce the environmental risk posed by persistent pollutants.

4. Conclusion

In this study, Cu-HNCN nanotube catalysts with highly dispersed and stable CuN_x sites were successfully constructed and applied to degrade antibiotic contaminants by the PF process. The catalyst exhibited excellent degradation performance without selectivity for complex water matrices. Stability studies confirmed that the CuNx sites were stably confined to the geometrically optimized Cu-HNCN because of planar bending caused by the nanotubes, which in turn led to short Cu-N bonds. Differential charge calculations indicated that the nanotubes enhanced the charge transfer. In addition, mechanistic investigation concluded that the excellent catalytic degradation capability was attributed to the nanotube properties, which enhanced the generation, separation, and transport of photogenerated electrons in Cu-HNCN, promoting the production of O2-, OH, h+, and 1O2. Moreover, based on FED calculations and LC-MS results, TET degradation pathways were proposed. Furthermore, the Cu-HNCN/PF system could effectively reduce the environmental risks caused by persistent pollutants. In summary, this study provides a new approach for improving the stability and accelerating the electron transfer of catalysts, while also providing a reference for the development of environmental functional materials

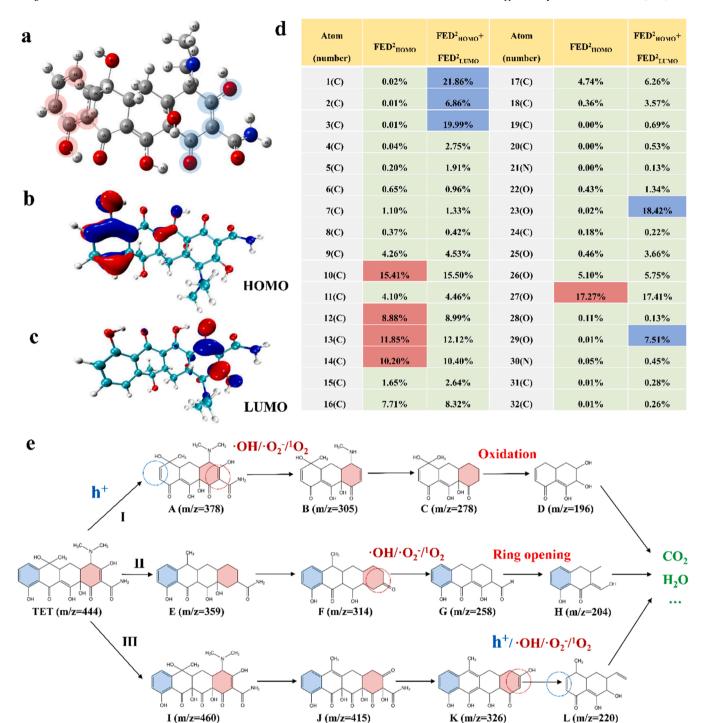


Fig. 10. (a) Optimized TET molecular configuration. (b) FEDs of HOMO of TET. (c) FEDs of LUMO of TET. (d) FEDs on atoms of TET. (e) Proposed pathways of TET degradation by Cu-HNCN/PF system.

and efficient wastewater purification technology.

CRediT authorship contribution statement

Xiao Zhang, Peng Yu, Yongjun Sun: Conceptualization, Methodology, Software, Writing – original draft, Resources, Investigation, Data curation. Xiao Zhang, Baokang Xu, Shiwen Wang, Xi Li, Cheng Wang, Yanhua Xu, Ru Zhou, Yang Yu, Huaili Zheng: Data curation. Xiao Zhang, Baokang Xu, Shiwen Wang, Xi Li, Cheng Wang: Investigation. Yanhua Xu, Yang Yu, Huaili Zheng, Peng Yu, Yongjun Sun: Resources. Xiao Zhang, Yang Yu, Huaili Zheng, Peng Yu, Yongjun

Sun: Investigation. Yanhua Xu, Yang Yu, Huaili Zheng, Peng Yu, Yongjun Sun: Supervision. Yanhua Xu, Yang Yu, Huaili Zheng, Peng Yu, Yongjun Sun: Conceptualization, Funding acquisition, Supervision; Xiao Zhang, Peng Yu, Yongjun Sun: Writing – review & editing, Funding acquisition, Supervision.

Declaration of Competing Interest

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

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Appendix A. Supporting information

Supplementary data associated with this article can be found in the online version at doi:10.1016/j.apcatb.2022.121119.

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